MARKED UP VERSION OF AMENDED CLAIMS

- 1. (Once Amended) A [P] process for the catalytic dewaxing of a hydrocarbon oil feed including waxy molecules and more than 500 ppmw of sulphur or sulphur containing compounds by contacting the oil feed under catalytic dewaxing conditions with a catalyst composition comprising a Group VIII metal hydrogenation component, dealuminated aluminosilicate zeolite crystallites and a low acidity refractory oxide binder material which is essentially free of alumina.
- 2. (Once Amended) The [P] process [according to] of claim 1, wherein the oil feed comprises more than 750 ppmw of sulphur or sulphur containing compounds.
- 3. (Once Amended) The [P] process [according to any one of claims 1-2,] of claim 1, [wherein] in which the oil feed comprises more than 10 ppmw of nitrogen or nitrogen containing compounds.
- 4. (Once Amended) The [P] process [according to any one of claims 1-3,] of claim 1, [wherein] in which the hydrogenation component is platinum[, palladium or nickel].

- 5. (Once Amended) The [P] process [according to any one of claims 1-4,] of claim 1, [wherein] in which the low acidity binder is silica.
- 6. (Once Amended) The [P] process [according to any one of claims 1-5,] of claim 1, [wherein] in which the aluminosilicate zeolite crystallites have a Constraint Index of between 2 and 12.
- 7. (Once Amended) The [P] process [according to] of claim 6, [wherein] in which the aluminosilicate zeolite crystallites is of the MFI type.

8. (Once Amended) The [P] process [according to any one of claims 1-7,] of claim 1, [wherein] in which the dealuminated aluminosilicate zeolite crystallites are obtained by contacting the zeolite crystallites with an aqueous solution of a fluorosilicate salt wherein the fluorosilicate salt is represented by the formula:

$$(A)_{2/b}SIF_6$$

[wherein] in which 'A' is a metallic or non-metallic cation other than H+ having the valence 'b'[, preferably ammonium].

- 9. (Once Amended) The [P] process [according to any one] of claim[s] 8, [wherein] in which an extrudate of the aluminosilicate zeolite crystallites and the low acidity binder is contacted with the aqueous solution of the fluorosilicate salt.
- 10. (Once Amended) The [P] process [according to any one of claims 1-9] of claims 1. (wherein] in which the oil feed is a solvent extracted waxy raffinate.
- 11. (Once Amended) The [P] process [according to any one of claims 1-9] of claim 1. [wherein] in which the oil feed is a gas oil.
- 12. (Once Amended) The [P] process [according to any one of claims 1-9] of claim 1, [wherein] in which the oil feed is a hydrocracker feedstock and wherein the dewaxed oil is subsequently subjected to a hydrocracker process step in which step primarily middle distillates are prepared.

13. (Once Amended) A method of [Method for] retrofitting a process for preparing lubricating base oils [wherein] in which an existing solvent dewaxing step is replaced by a catalytic dewaxing process comprising the steps of contacting the oil feed under catalytic dewaxing conditions with a catalyst composition comprising a Group VIII metal hydrogenation component, dealuminated aluminosilicate zeolite crystallites and a low acidity refractory oxide binder material which is essentially free of alumina [according to any one] of [claims 1 to 10.] claim 1.

Please add new claims 14, 15 and 16:

14. The process of claim 8, where 'b' is ammonium.

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- 15. The process of claim 1, in which the hydrogenation component is palladium.
- 16. The process of claim 1, in which the hydrogenation component is nickel the process of claim 1.